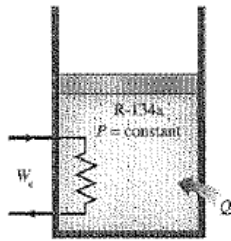


Cankaya University
Faculty of Engineering
Mechanical Engineering Department
ME 211 Thermodynamics I
Closed Notes and Books

26.12.2015

Show all steps of your work to get partial credit

1) A mass of 12 kg of saturated refrigerant-134a vapor is contained in a piston-cylinder device at 240 kPa. Now 300 kJ of heat is transferred to the refrigerant at constant pressure while a 110-V source supplies current to a resistor within the cylinder for 6 min. Determine the current supplied if the final temperature is 70 °C. Also, show the process on a T-v diagram with respect to the saturation lines.



closed system $\Delta KE = \Delta PE = 0$

$$Q - W = m(u_2 - u_1)$$

$$Q - W_e - W_b = m(u_2 - u_1)$$

$$W_b = \int_1^2 p \, dv = m p (v_2 - v_1) = m (P_2 v_2 - P_1 v_1)$$

so

$$Q - W_e = m(h_2 - h_1)$$

$$W_e = VI \Delta t$$

$$P_1 = 240 \text{ kPa} = 2.4 \text{ bar} \quad] \quad h_1 = h_g = 244.09 \text{ kJ/kg}$$

$$x_1 = 1$$

$$P_2 = 240 \text{ kPa} \quad] \quad h_2 = 313.49 \text{ kJ/kg}$$

$$T_1 = 70^\circ \text{C}$$

$$W_e = Q - m(h_2 - h_1) = 300 - 12(313.49 - 244.09)$$

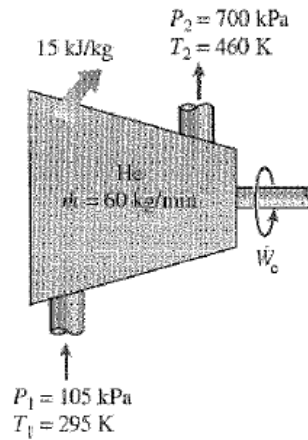
$$= -532.8 \text{ kJ} \leftarrow \text{work done on system}$$

$$I = (-532.8)^{1/3} / [110(6 \text{ min}) \left(\frac{60 \text{ s}}{\text{min}} \right)] = 13.45 \text{ A}$$

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2) Helium is to be compressed from 105 kPa and 295 K to 700 kPa and 460 K. A heat loss of 15 kJ/kg occurs during the compression process. Neglecting kinetic and potential energy changes, determine the power input required for a mass flow rate of 60 kg/min. Assume that Helium is ideal gas and the constant pressure specific heat of helium is $c_p = 5.1926 \text{ kJ/kg}\cdot\text{K}$. Do not use Tables.



SSSF
 $\Delta KE = 0$ $\Delta PE = 0$
 $\dot{m} = 60 \text{ kg/min} = 1 \text{ kg/s}$
 $q = 15 \text{ kJ/kg}$

$$\dot{Q}_{cv} - \dot{W}_{cv} = \dot{m}(h_2 - h_1)$$

$$\dot{W}_{cv} = \dot{Q}_{cv} - \dot{m}(h_2 - h_1) = \dot{m}q - \dot{m}(h_2 - h_1)$$

$$= (\dot{m}q) - \dot{m}c_p(T_2 - T_1)$$

$$= \left(60 \frac{\text{kg}}{\text{min}}\right) \left(\frac{\text{min}}{60\text{s}}\right) \left[-15 \frac{\text{kJ}}{\text{kg}} - 5.1926 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} (460 - 292)\right]$$

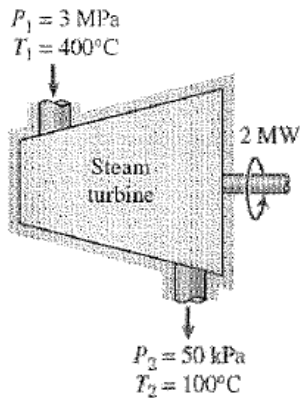
$$= -871 \text{ kW}$$

$$\frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

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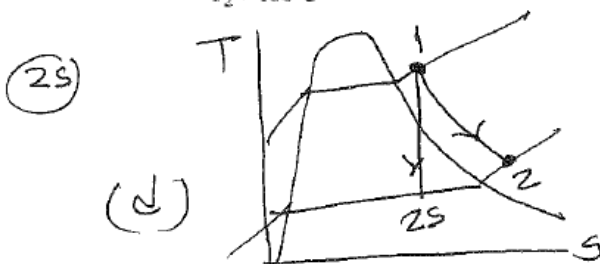
- 3) Steam enters an adiabatic turbine steadily at 3 MPa and 440 °C and leaves at 100 kPa and 100 °C. If the power output of the turbine is 2 MW, determine:
- the isentropic efficiency of the turbine
 - the mass flow rate of the steam flowing through the turbine.
 - entropy generation rate within the turbine
 - show the process on a T-S diagram with respect to saturation lines



SSSF $\Delta KE=0$ $\Delta PE=0$

$$P_1 = 30 \text{ bar} \left. \begin{array}{l} h_1 = 3321.5 \text{ kJ/kg} \\ T_1 = 440^\circ\text{C} \end{array} \right\} s_1 = 7.0520 \text{ kJ/kg K}$$

$$P_2 = 1 \text{ bar} \left. \begin{array}{l} s_2 = 7.3614 \text{ kJ/kg} \\ T_2 = 100^\circ\text{C} \end{array} \right\} h_2 = 2676.2 \text{ kJ/kg}$$



$$P_{2s} = 1 \text{ bar}$$

$$s_{2s} = s_1 = 7.052 \text{ kJ/kg}$$

$$s_g = 7.3594 \text{ kJ/kg}$$

$$s_f = 1.3026 \text{ kJ/kg}$$

$$7.052 = 1.3026 + x_{2s} (7.3594 - 1.3026) \quad x_{2s} = 0.949$$

$$h_{2s} = h_f + x_{2s} h_{fg} = 417.46 + 0.949 (2258) = 2560.3 \text{ kJ/kg}$$

$$\eta_t = \frac{\dot{W}}{\dot{W}_s} = \frac{h_1 - h_2}{h_1 - h_{2s}} = \frac{(3321.5 - 2676.2)}{(3321.5 - 2560.3)} = 0.84$$

$$b) -\dot{W} = \dot{m} (h_2 - h_1) \Rightarrow \dot{m} = \frac{(2000 \text{ kJ/s})}{2676.2 - 3321.5} = 3.09 \text{ kg/s}$$

$$c) \dot{\sigma} = \dot{m} (s_2 - s_1) = (3.09) (7.3614 - 7.052) = 0.95 \text{ kJ/K}$$

