

Çankaya University
Faculty of Engineering
Mechanical Engineering department
ME 211 Thermodynamics I
Midterm Exam 1
23.11.2017- SOLUTION

- 1) Nitrogen expands in a piston-cylinder system from 690 kPa and 260 °C to 210 kPa and 40 °C. Assuming ideal gas behavior, calculate the work done by the nitrogen. Assume pressure and volume are related by $pV^n = \text{const}$, where n is exponent.

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{n-1}{n}}$$

$$\Rightarrow \frac{313}{533} = \left(\frac{210}{690}\right)^{\frac{n-1}{n}}$$

$$\Rightarrow 0,5872 = 0,3043^{\frac{n-1}{n}} \quad (\text{take ln of both sides})$$

$$\ln(0,5872) = \frac{n-1}{n} \cdot \ln(0,3043) \Rightarrow \frac{n-1}{n} = 0,447$$

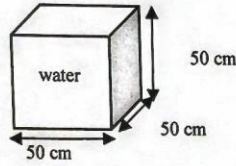
$$\Rightarrow 0,447n = n - 1 \Rightarrow n = \frac{1}{0,5525} \Rightarrow \underline{\underline{n = 1,81}}$$

$$W = \int_{V_1}^{V_2} P dV = \int_{V_1}^{V_2} \frac{C}{V^n} dV = \frac{(P_2 V_2 - P_1 V_1)}{1-n} \quad R = \frac{\bar{R}}{M} = \frac{8,314}{28} = 0,2968 \frac{\text{kJ}}{\text{kg}}$$

From ideal gas eqn: $PV = mRT$

$$w = \int_{T_1}^{T_2} \frac{R \cdot (T_2 - T_1)}{1-n} = \frac{0,2968 \cdot (313 - 533)}{1 - 1,81} = \underline{\underline{80 \text{ kJ/kg}}}$$

- 2) A rigid cubic container, 50 cm on each side, contains a wet mixture of water vapor at 90°C and 20 percent quality. Heat is added until the pressure is raised to 500 kPa. Determine the final temperature and the quantity of heat added.



$$V = 0,125 \text{ m}^3$$

$$v = \frac{V}{m}$$

$$m = \frac{V}{v_1} = \frac{0,125}{0,473} = \underline{\underline{0,2643 \text{ kg}}}$$

$$u_f = 376,85 \text{ kJ/kg}, \quad u_g = 2494,5 \text{ kJ/kg}$$

$$u_1 = u_f + x(u_g - u_f) = 376,85 + 0,2(2494,5 - 376,85)$$

$$\underline{\underline{u_1 = 800,38 \text{ kJ/kg}}}$$

State 1

$$T_1 = 90^\circ\text{C}, \quad x_1 = 0,2 \quad (\text{Table A.2})$$

$$v_f = 1,036 \cdot 10^{-3} \text{ m}^3/\text{kg}$$

$$v_g = 2,361 \text{ m}^3/\text{kg}$$

$$v_1 = v_f + x(v_g - v_f)$$

$$\Rightarrow v_1 = 1,036 \cdot 10^{-3} + 0,2(2,361 - 1,036 \cdot 10^{-3})$$

$$\Rightarrow \underline{\underline{v_1 = 0,473 \text{ m}^3/\text{kg}}}$$

State 2 $P_2 = 500 \text{ kPa}$, $v_2 = v_1 = 0,473 \text{ m}^3/\text{kg}$

(Table A.3) $P = 5 \text{ bar}$, $v_f = 1,0926 \cdot 10^{-3} \text{ m}^3/\text{kg}$

$$v_g = 0,3749 \text{ m}^3/\text{kg}$$

$v_2 > v_g \Rightarrow$ superheated!

(Table A-4) $P = 5 \text{ bar}$.

$T(^{\circ}\text{C})$	$v \text{ (m}^3/\text{kg)}$	$u \text{ (kJ/kg)}$
240	0,4646	2707,6
$T_2 = ?$	$v_2 = 0,473$	$u_2 = ?$
280	0,5034	2771,2

Interpolation: $\underline{\underline{T_2 \approx 244^\circ\text{C}}}$ and $\underline{\underline{u_2 = 2720,9 \text{ kJ/kg}}}$

1st Law: $\Delta U = 1Q_2 - 1W_2 \Rightarrow m(u_2 - u_1) = 1Q_2$

$$1Q_2 = 0,2643(2720,9 - 800,38) \Rightarrow \underline{\underline{1Q_2 = 507,6 \text{ kJ}}}$$

3) A piston cylinder arrangement with a linear spring as shown in the figure contains R-134a at 12°C , $x=0.4$ and a volume of 0.02 m^3 . It is then heated to 60°C at which point specific volume is $0.04134\text{ m}^3/\text{kg}$. Find the final pressure, the work and heat transfer in the process. Show the p-v diagram with respect to saturation lines.



State 1

$$T_1 = 12^\circ\text{C}, x = 0.4 \text{ (sat. mix)}$$

(Table A.10) $v_f = 0.7971 \cdot 10^{-3}\text{ m}^3/\text{kg}$
 $v_g = 0.0460\text{ m}^3/\text{kg}$

$$v_1 = v_f + x(v_g - v_f)$$

$$v_1 = 0.7971 \cdot 10^{-3} + 0.4(0.046 - 0.7971 \cdot 10^{-3})$$

$$\Rightarrow v_1 = 0.0192\text{ m}^3/\text{kg}$$

$$u_f = 65.83\text{ kJ/kg}, u_g = 233.63\text{ kJ/kg}$$

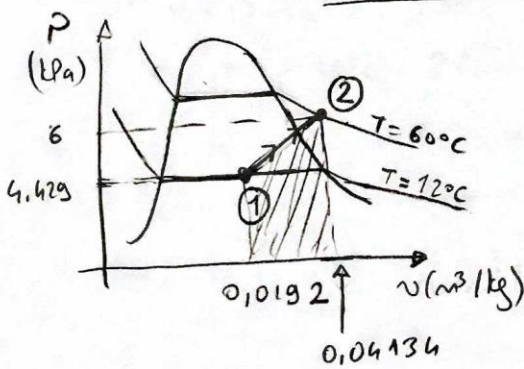
$$u_1 = 65.83 + 0.4(233.63 - 65.83) = 132.95\text{ kJ/kg}$$

$$m = V_1/v_1 = 0.02/0.0192 \Rightarrow m = 1.041\text{ kg}$$

State 2

$$T_2 = 60^\circ\text{C} \text{ and } v_2 = 0.04134\text{ m}^3/\text{kg} \Rightarrow \text{Superheated}$$

(Table A.12) $P_2 = 6\text{ bar} = 600\text{ kPa}, u_2 = 273.54\text{ kJ/kg}$



$${}_1W_2 = \int_{v_1}^{v_2} p dv = m \int_{v_1}^{v_2} p dv$$

(Area of the trapezoid)

$${}_1W_2 = \frac{1.041}{2} \cdot [(600 + 442.9)(0.04134 - 0.0192)]$$

$$\Rightarrow {}_1W_2 = 12.02\text{ kJ}$$

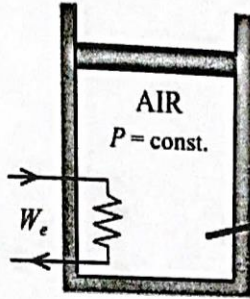
Energy balance:

$$\Delta u = m(u_2 - u_1) = {}_1Q_2 - {}_1W_2 \Rightarrow {}_1Q_2 = m(u_2 - u_1) + {}_1W_2$$

$$\Rightarrow {}_1Q_2 = 1.041 \cdot (273.54 - 132.95) + 12.02$$

$$\Rightarrow {}_1Q_2 = 158.37\text{ kJ}$$

4.) A mass of 15 kg of air in a piston-cylinder device is heated from 25 °C to 77 °C by passing electric current through a resistance heater inside the cylinder. The pressure inside the cylinder is held constant at 300 kPa during the process, and a heat loss of 60 kJ occurs. Determine the electric energy supplied in kWh. (1 kWh=3600 kJ)



Energy balance:

$$\Delta U = 1\phi_2 - [W_e + W_b]$$

$$1\phi_2 - W_e = m(u_2 - u_1) + W_b$$

$$\text{where } W_b = \int_{V_1}^{V_2} P dV = P_2 V_2 - P_1 V_1$$

$$\Rightarrow 1\phi_2 - W_e = \underbrace{m(u_2 - u_1) + m(P_2 v_2 - P_1 v_1)}_{m(h_2 - h_1)}$$

$$\Rightarrow 1\phi_2 - W_e = m(h_2 - h_1)$$

• 1st way: (variable c_p)

$$\text{(Table A.22)} \quad T_1 = 25^\circ\text{C} = 298 \text{ K} \Rightarrow h_1 = 298 \text{ kJ/kg}$$

$$T_2 = 77^\circ\text{C} = 350 \text{ K} \Rightarrow h_2 = 350.5 \text{ kJ/kg}$$

$$\Rightarrow -60 - W_e = 15 \cdot (350.49 - 298)$$

$$\Rightarrow -W_e = 847.35 \Rightarrow \underline{\underline{W_e = -847.35 \text{ kJ}}}$$

$$\underline{\text{electrical energy}} := (-847.35) = \underline{\underline{847.35 \text{ kJ}}}$$

$$W_{\text{elect}} = 847.35 \text{ kJ} \left[\frac{\text{kWh}}{3600 \text{ kJ}} \right] = \underline{\underline{0.235 \text{ kWh}}}$$

• 2nd way: $T_{\text{avg}} = \frac{298 + 350}{2} \approx 325 \text{ K} \Rightarrow c_p = 1.0065 \text{ kJ/kgK}$

$$\text{(const)} \quad 1\phi_2 - W_e = m \cdot c_p \cdot (T_2 - T_1)$$

$$-60 - W_e = 15 \cdot 1.0065 (350 - 298)$$

$$\underline{\underline{W_e = -845.1 \text{ kJ}}}, \quad \underline{\underline{W_{\text{elect}} = 0.235 \text{ kWh}}}$$