

Steam Tables Tutorial

(Illustration of Steam Tables Process Overview)

Example 1 (p and T given)

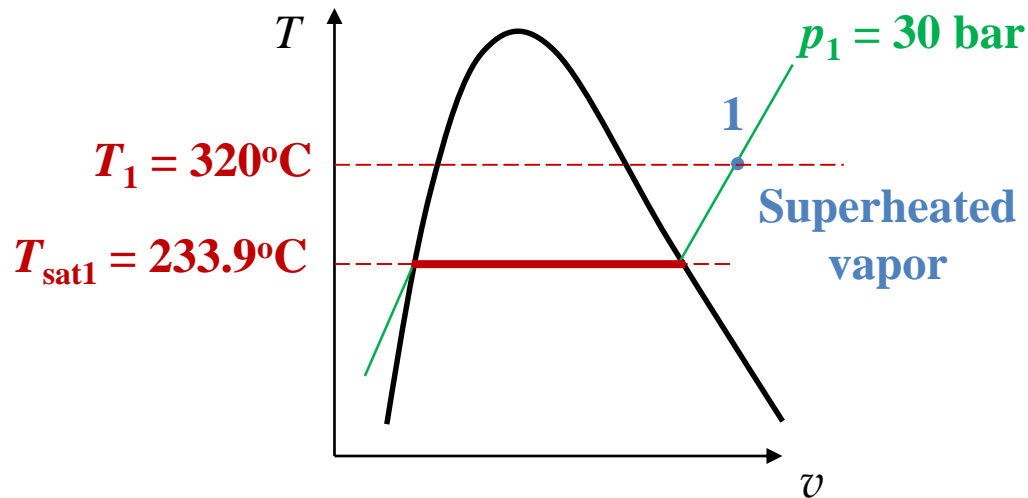
Given: $p_1 = 30 \text{ bar}$, $T_1 = 320^\circ\text{C}$

From Table A-3 @ $p_1 = 30 \text{ bar}$

$T_{\text{sat1}} = 233.9^\circ\text{C}$

Conclusion: Since $T_1 > T_{\text{sat1}}$,

- State 1 is **Superheated vapor**
- Obtain properties from **Table A-4**



Example 1 (p and T given)

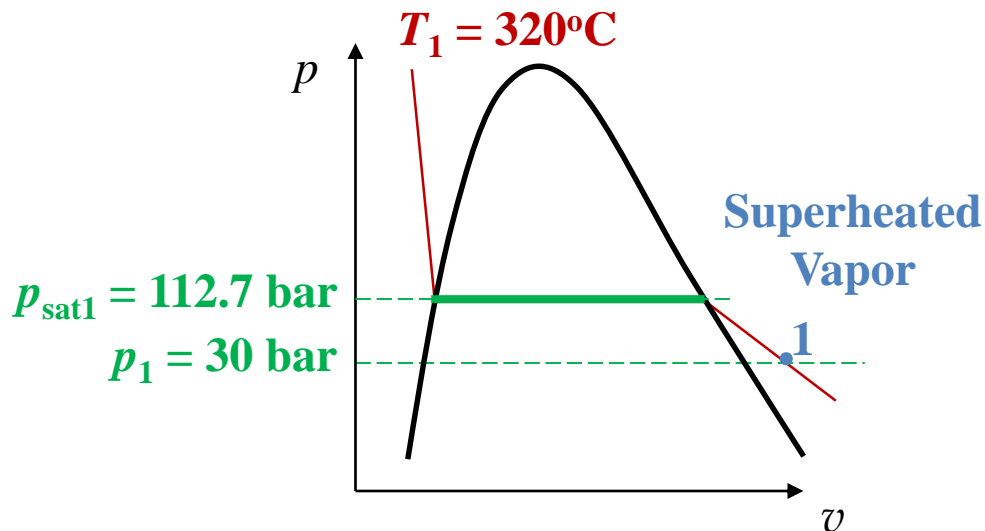
Given: $p_1 = 30 \text{ bar}$, $T_1 = 320^\circ\text{C}$

From Table A-2 @ $T_1 = 320^\circ\text{C}$

$$p_{\text{sat}1} = 112.7 \text{ bar}$$

Conclusion: Since $p_1 < p_{\text{sat}1}$,

- State 1 is **Superheated vapor**
- Obtain properties from **Table A-4**



Example 2 (p and T given)

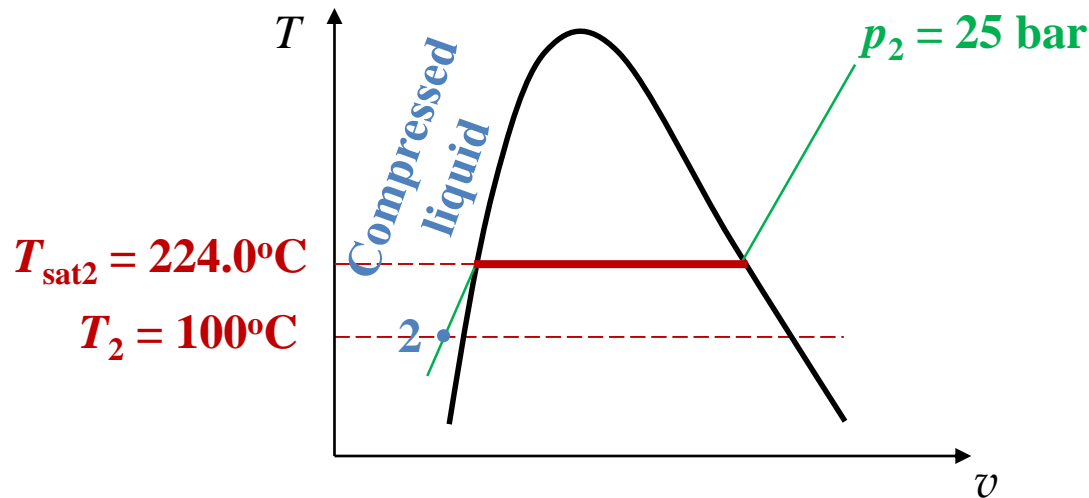
Given: $p_2 = 25$ bar, $T_2 = 100^\circ\text{C}$

From Table A-3 @ $p_2 = 25$ bar

$T_{\text{sat}2} = 224.0^\circ\text{C}$

Conclusion: Since $T_2 < T_{\text{sat}2}$,

- State 2 is **Compressed liquid**
- Obtain properties from **Table A-5** or **A-2** (approximate as **saturated liquid**)



Example 2 (p and T given)

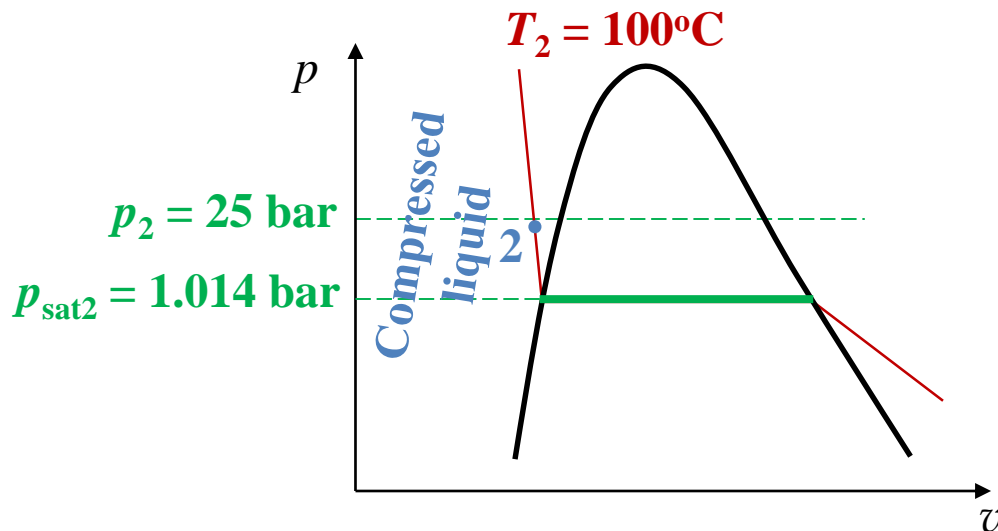
Given: $p_2 = 25 \text{ bar}$, $T_2 = 100^\circ\text{C}$

From Table A-2 @ $T_2 = 100^\circ\text{C}$

$$p_{\text{sat}2} = 1.014 \text{ bar}$$

Conclusion: Since $p_2 > p_{\text{sat}2}$,

- State 2 is **Compressed liquid**
- Obtain properties from **Table A-5** or **Table A-2** (approximate as saturated liquid)



Example 3 (p and T given)

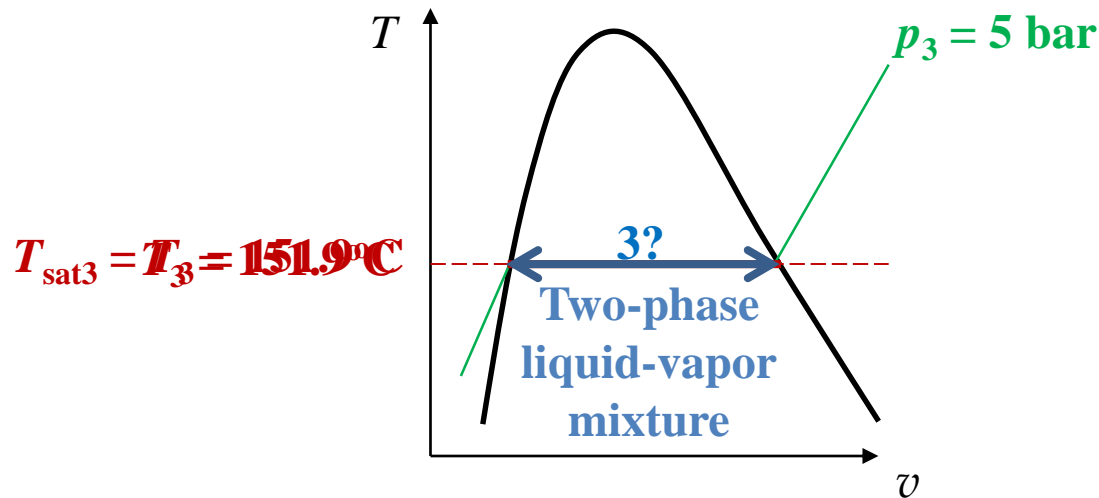
Given: $p_3 = 5 \text{ bar}$, $T_3 = 151.9^\circ\text{C}$

From Table A-3 @ $p_3 = 5 \text{ bar}$

$T_{\text{sat}3} = 151.9^\circ\text{C}$

Conclusion: Since $T_3 = T_{\text{sat}3}$,

- State 3 is **Two-phase liquid-vapor mixture**
- **Need another property** to obtain properties



Example 4 (p and T given)

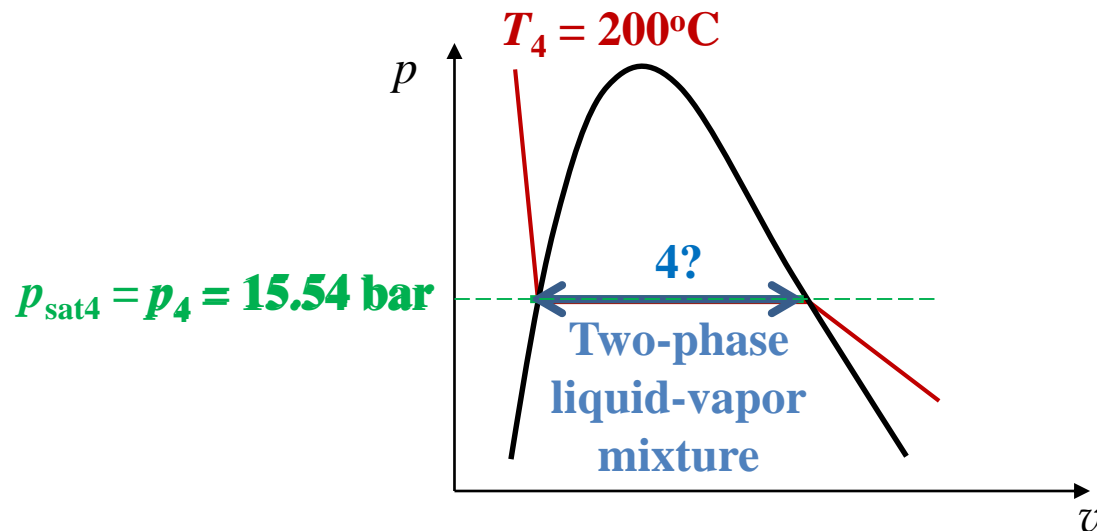
Given: $p_4 = 15.54$ bar, $T_4 = 200^\circ\text{C}$

From Table A-2 @ $T_4 = 200^\circ\text{C}$

$$p_{\text{sat}4} = 15.54 \text{ bar}$$

Conclusion: Since $p_4 = p_{\text{sat}4}$,

- State 4 is **Two-phase liquid-vapor mixture**
- **Need another property** to obtain properties



Example 5 (T and v given)

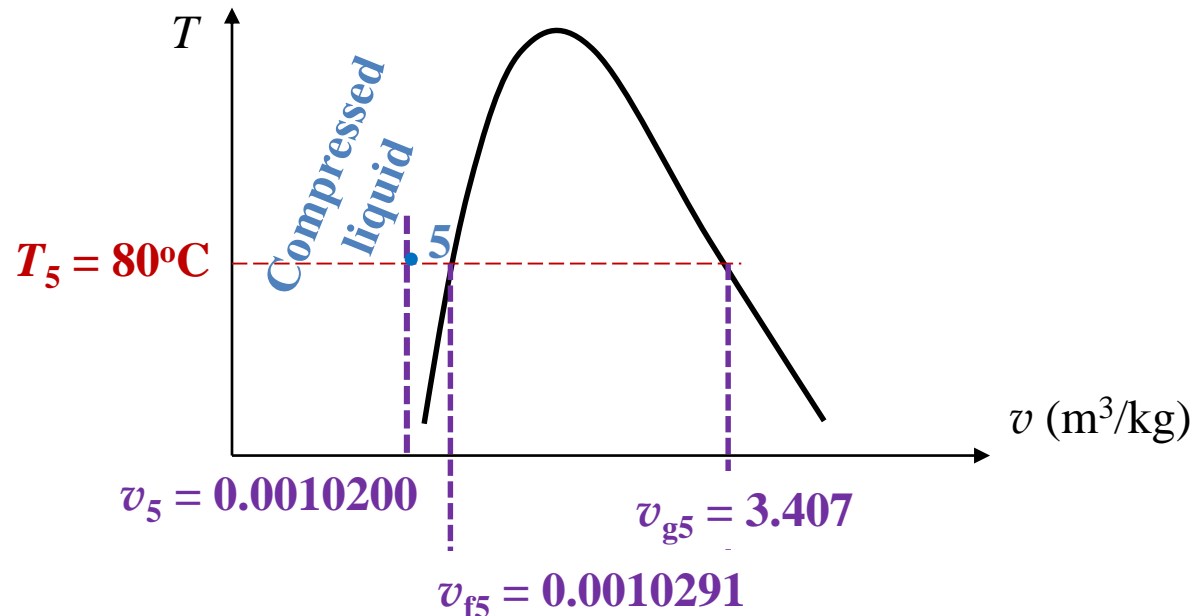
Given: $T_5 = 80^\circ\text{C}$ and $v_5 = 0.0010200 \text{ m}^3/\text{kg}$

From Table A-2 @ $T_5 = 80^\circ\text{C}$

$v_{f5} = 0.0010291 \text{ m}^3/\text{kg}$ and $v_{g5} = 3.407 \text{ m}^3/\text{kg}$

Conclusion: Since $v_5 < v_{f5}$,

- State 5 is **Compressed liquid**
- Obtain properties from **Table A-5** or **Table A-2 (approximate as saturated liquid)**



Example 6 (T and v given)

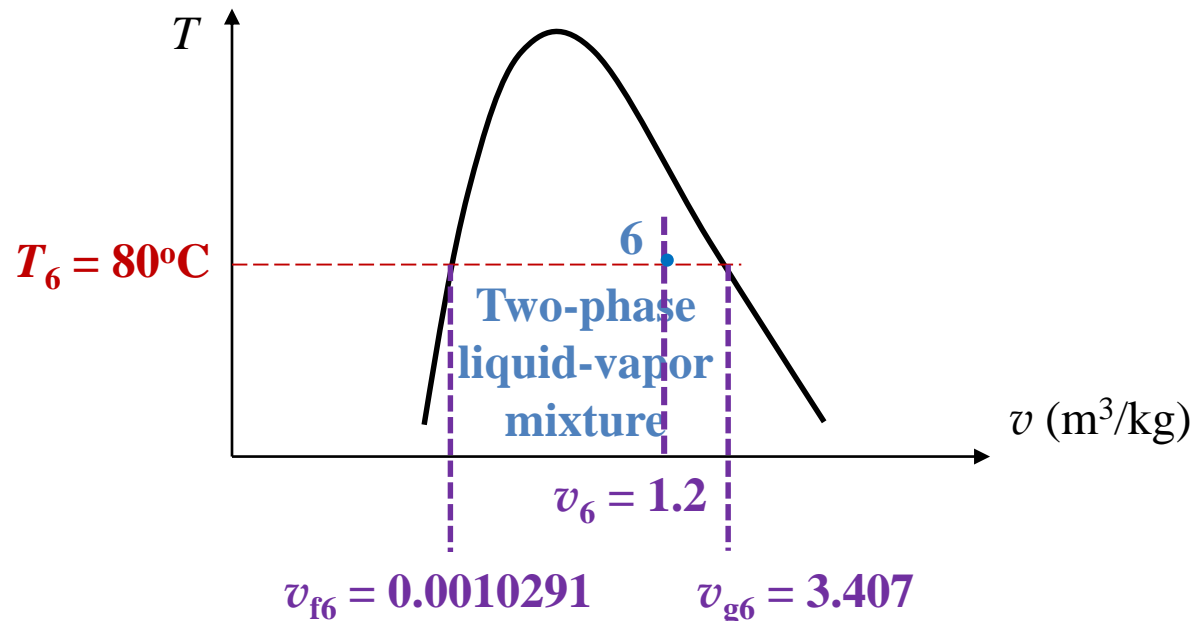
Given: $T_6 = 80^\circ\text{C}$ and $v_6 = 1.2 \text{ m}^3/\text{kg}$

From Table A-2 @ $T_6 = 80^\circ\text{C}$

$v_{f6} = 0.0010291 \text{ m}^3/\text{kg}$ and $v_{g6} = 3.407 \text{ m}^3/\text{kg}$

Conclusion: Since $v_{f6} < v_6 < v_{g6}$,

- State 6 is **Two-phase liquid-vapor mixture**
- Determine **quality (x_6)** and use quality calculations to compute desired properties



Example 7 (T and v given)

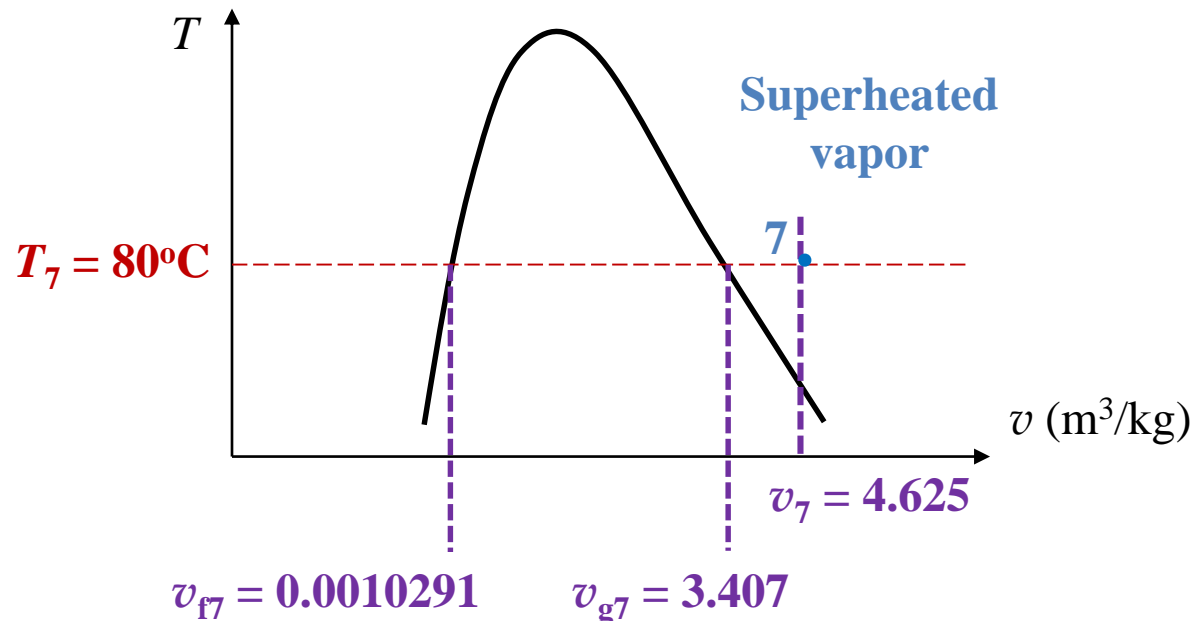
Given: $T_7 = 80^\circ\text{C}$ and $v_7 = 4.625 \text{ m}^3/\text{kg}$

From Table A-2 @ $T_7 = 80^\circ\text{C}$

$v_{f7} = 0.0010291 \text{ m}^3/\text{kg}$ and $v_{g7} = 3.407 \text{ m}^3/\text{kg}$

Conclusion: Since $v_7 > v_{g7}$,

- State 7 is **Superheated vapor**
- Obtain properties from **Table A-4**



Example 8 (p and u given)

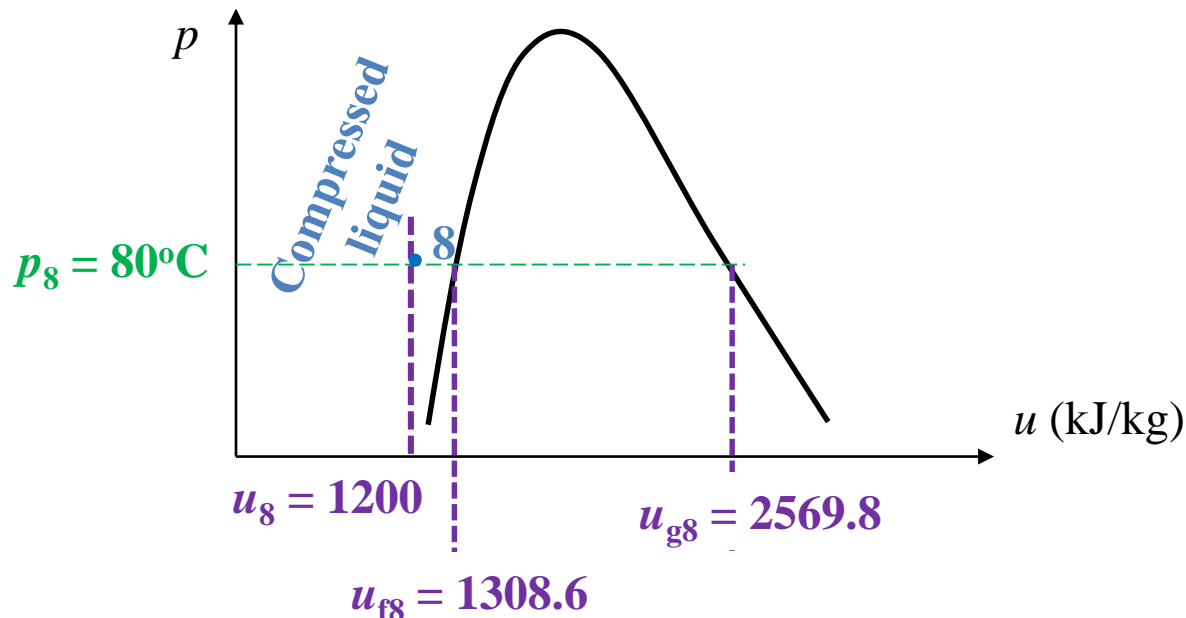
Given: $p_8 = 80$ bar and $u_8 = 1200$ m³/kg

From Table A-3 @ $p_8 = 80$ bar

$u_{f8} = 1308.6$ kJ/kg and $u_{g8} = 2569.8$ kJ/kg

Conclusion: Since $u_8 < u_{f8}$,

- State 8 is **Compressed liquid**
- Obtain properties from **Table A-5** or **Table A-2** (approximate as saturated liquid)



Example 9 (p and u given)

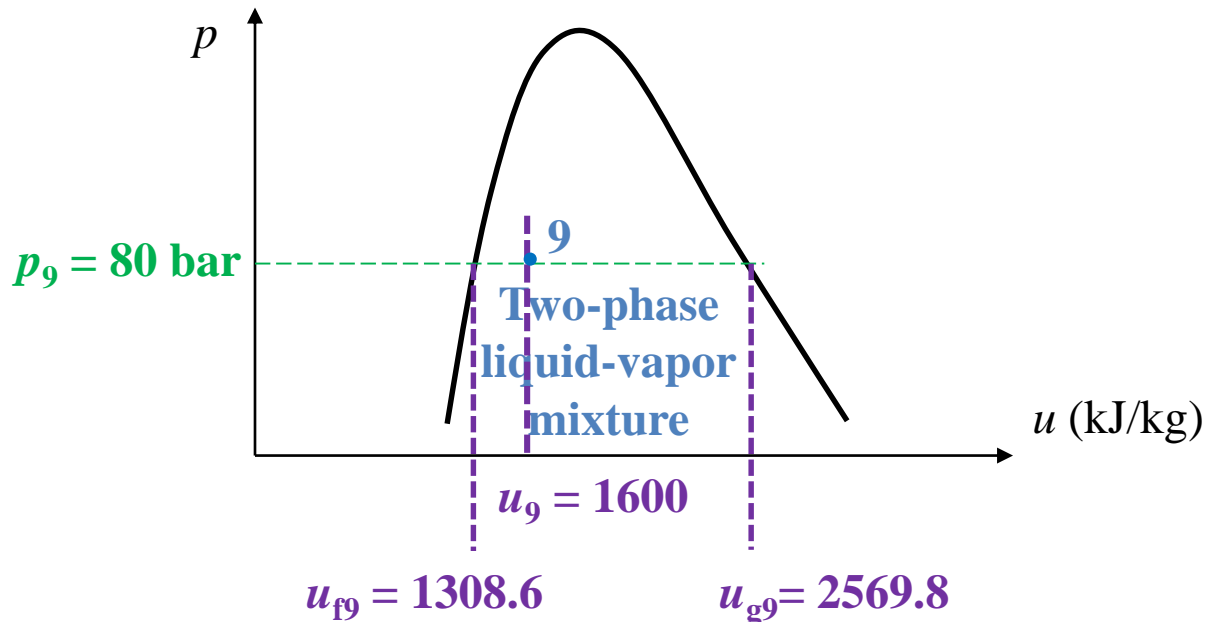
Given: $p_9 = 80$ bar and $u_9 = 1600$ kJ/kg

From Table A-3 @ $p_9 = 80$ bar

$u_{f9} = 1308.6$ kJ/kg and $u_{g9} = 2569.8$ kJ/kg

Conclusion: Since $u_{f9} < u_9 < u_{g9}$,

- State 9 is **Two-phase liquid-vapor mixture**
- Determine **quality (x_9)** and use quality calculations to compute desired properties



Example 10 (p and u given)

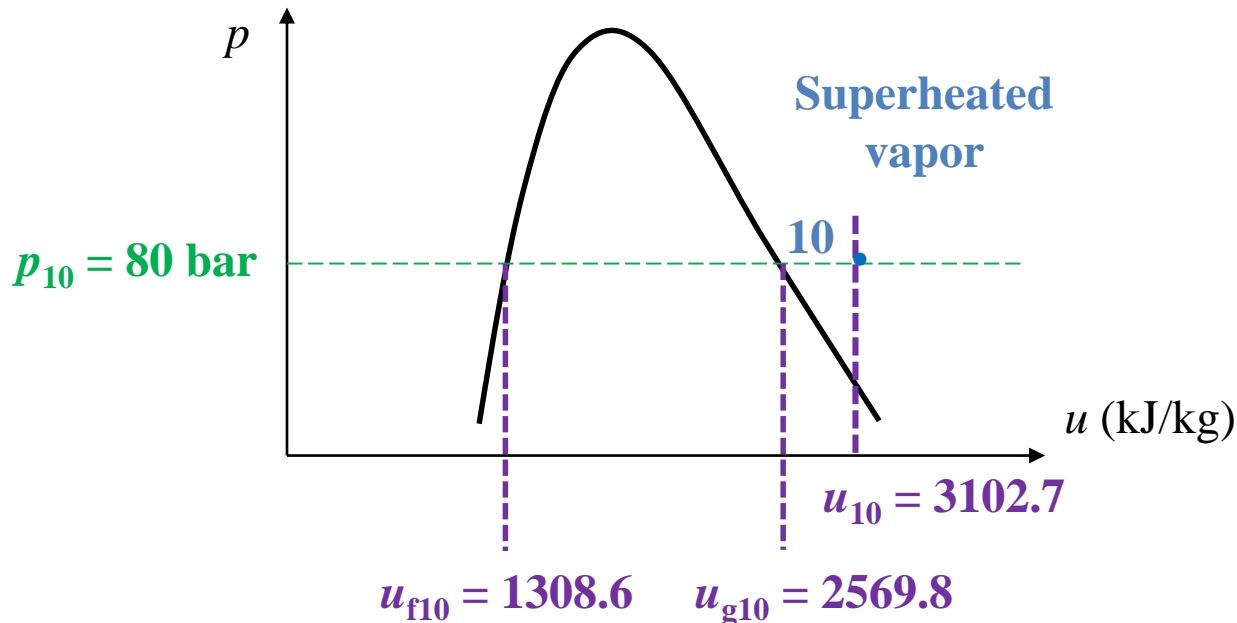
Given: $p_{10} = 80$ bar and $u_{10} = 3102.7$ kJ/kg

From Table A-3 @ $p_{10} = 80$ bar

$u_{f10} = 1308.6$ kJ/kg and $u_{g10} = 2569.8$ kJ/kg

Conclusion: Since $u_{10} > u_{g10}$,

- State 10 is **Superheated vapor**
- Obtain properties from **Table A-4**



Example 11 (T and x given)

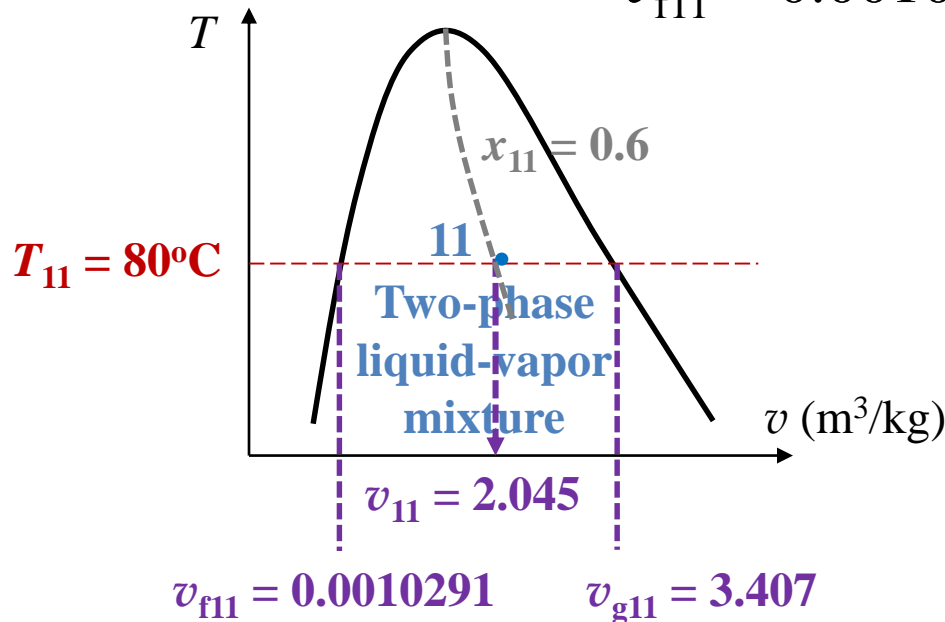
Given: $T_{11} = 80^\circ\text{C}$ and $x_{11} = 0.6$

Conclusion:

- State 11 is **Two-phase liquid-vapor mixture**
- Use **quality calculations** with **saturated liquid (f)** and **saturated vapor (g)** values from **Table A-2** to compute desired properties

From Table A-2 @ $T_{11} = 80^\circ\text{C}$

$$v_{f11} = 0.0010291 \text{ m}^3/\text{kg} \text{ and } v_{g11} = 3.407 \text{ m}^3/\text{kg}$$



$$v_{11} = v_{f11} + x_{11}(v_{g11} - v_{f11})$$

$$v_{11} = 2.045 \text{ m}^3/\text{kg}$$

Example 12 (p and x given)

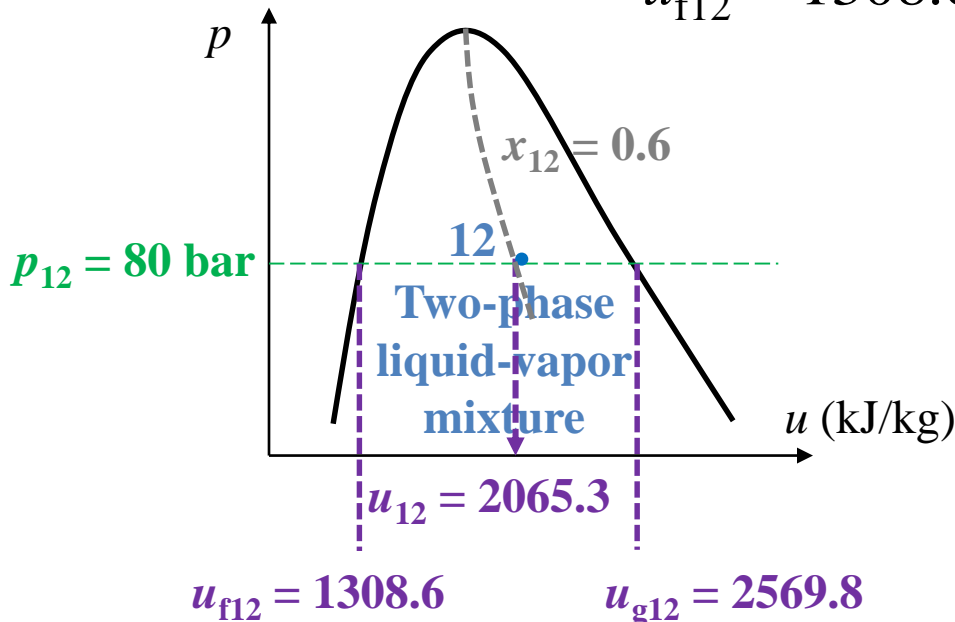
Given: $p_{12} = 80$ bar and $x_{12} = 0.6$

Conclusion:

- State 12 is **Two-phase liquid-vapor mixture**
- Use **quality calculations** with **saturated liquid (f)** and **saturated vapor (g)** values from **Table A-3** to compute desired properties

From Table A-3 @ $p_{12} = 80$ bar

$$u_{f12} = 1308.6 \text{ kJ/kg and } u_{g12} = 2569.8 \text{ kJ/kg}$$



$$u_{12} = u_{f12} + x_{12}(u_{g12} - u_{f12})$$

$$u_{12} = 2065.3 \text{ kJ/kg}$$